

# Development of effective purification method for peptides and proteins by silica gel based reversed phase packing material



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# Introduction

Reversed-phase HPLC is an invaluable tool for the analytical and preparative separation of peptides and proteins. Owing to the availability of different pore sizes and particle sizes, the alkyl-bonded silica gel products are economically the first choice for both analytical and preparative separations.

We reported that optimum pore size of gel gave good peak shape and good separation in analytical and preparative/process scale. Based on these results, we attempted to purify insulin with cost effectively. Actually, in the production by chromatography, cost performance would be most important thing. This study, we show cost-effective purification of insulin by optimizing necessary factors.



# Comparison of *preparative* and *analytical* chromatography

## Analytical

Peak shape  
Peak resolution  
Column choice  
Analytical time

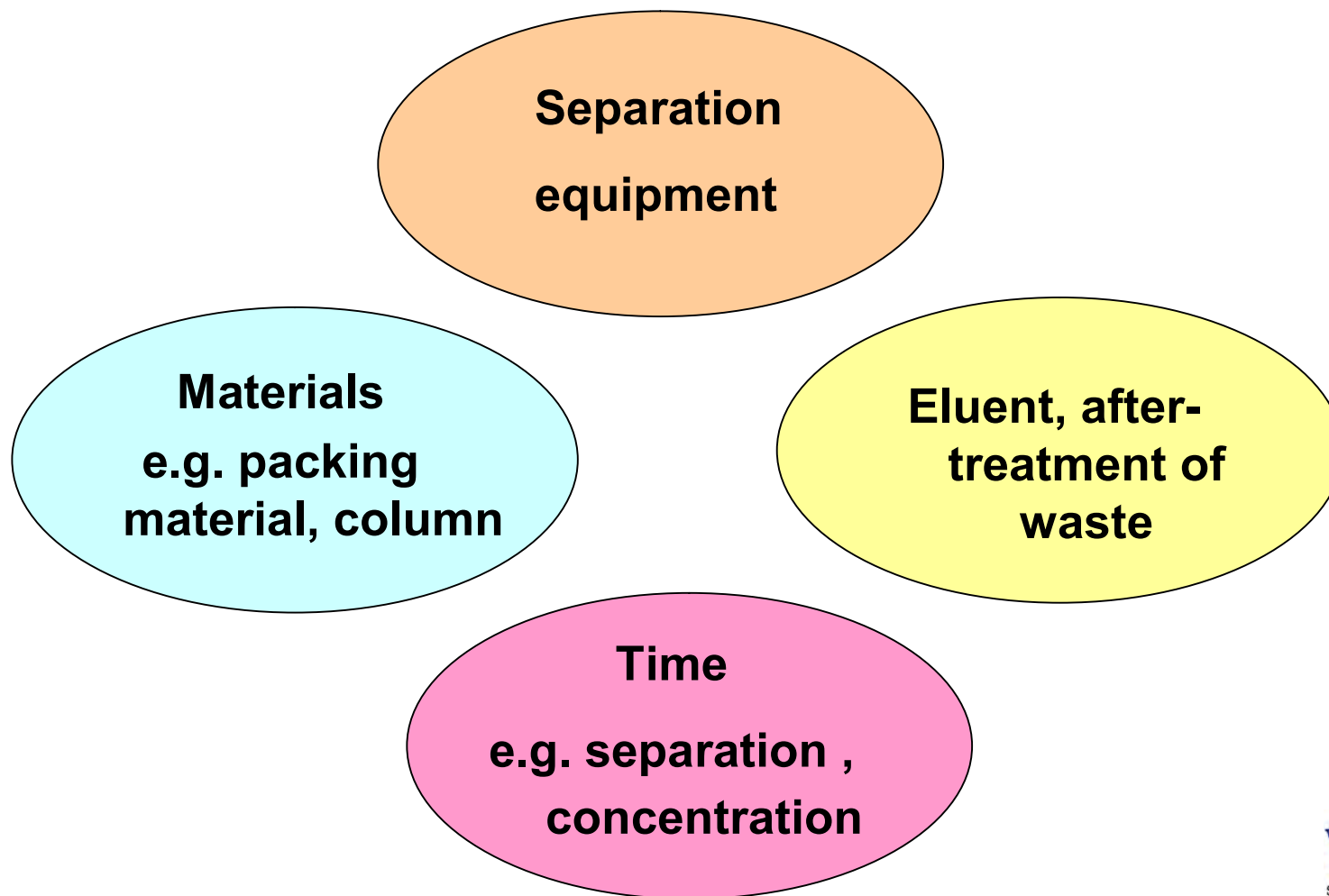
## Preparative

Recovery  
Purity  
*Cost performance*  
Safety in production

*In preparative scale, factors to be considered are*  
easily recovery, cycle time, recovery, purity, loading amount,  
solvent, etc.



# Preparative production cost includes





# Flow chart of preparative chromatography

**Set up separation conditions**  
(eluent, time of interval, flow rate, etc)



Choosing **packing material** (functional group)



Choosing **particle size**



Optimization of **preparative conditions**

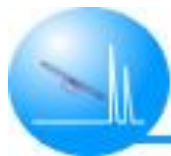


***Preparative chromatography***



## Recommend combination of MW and pore size for peptides and proteins

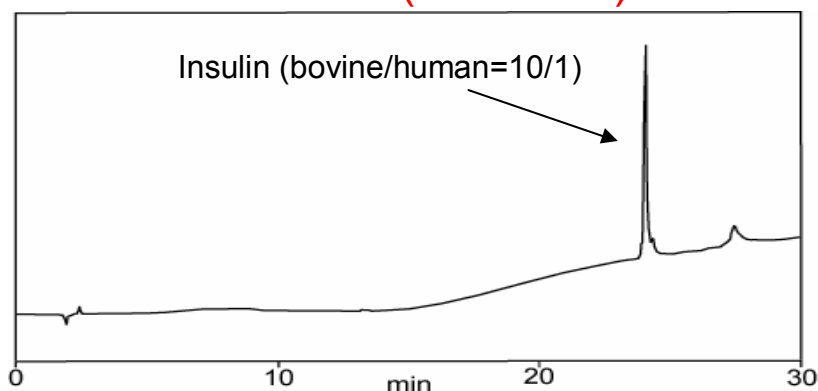
MW		C18	C8	C4
500	<b>Pore size</b> <b>120 Å</b>	⊙	○	△
5000	<b>200 Å</b>	○	⊙	○
20000	<b>300 Å</b>	△	○	⊙
100000				



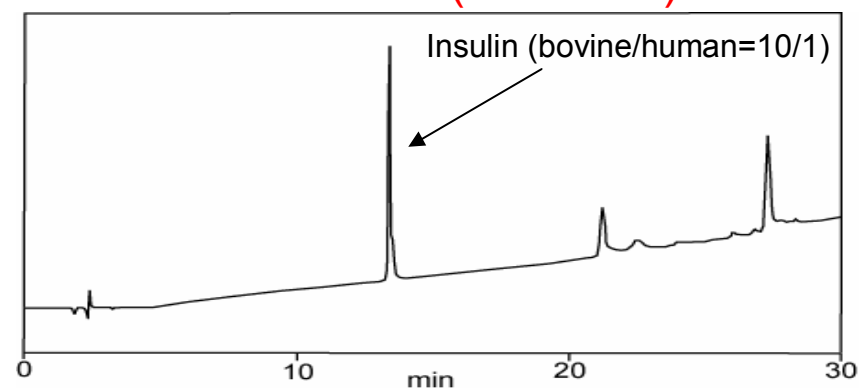
# Initial conditions for separation of insulin

## *comparison of solvent, MeOH vs ACN*

**Methanol (10-90%B)**



**Acetonitrile (10-90%B)**



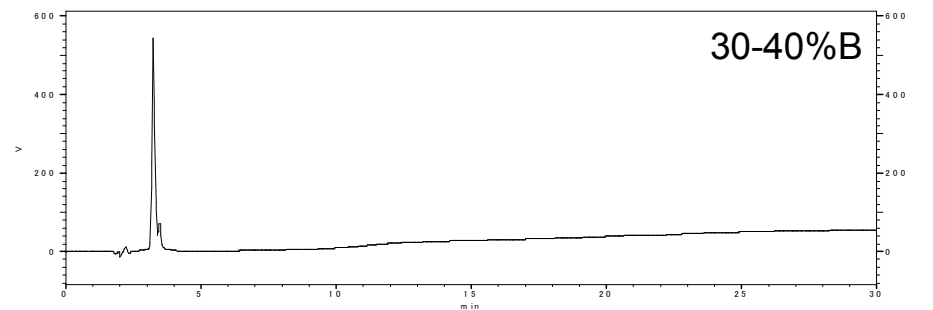
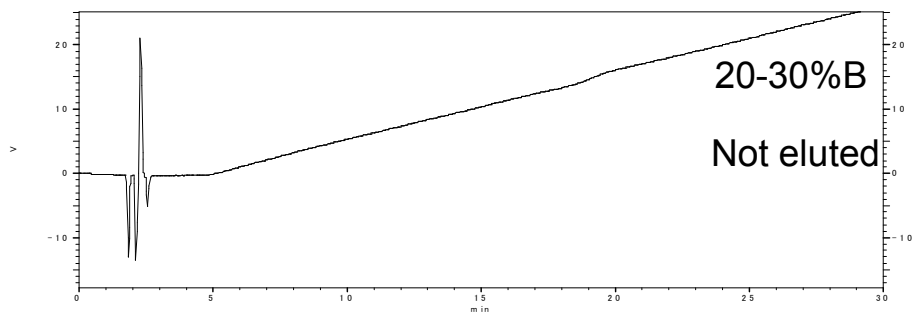
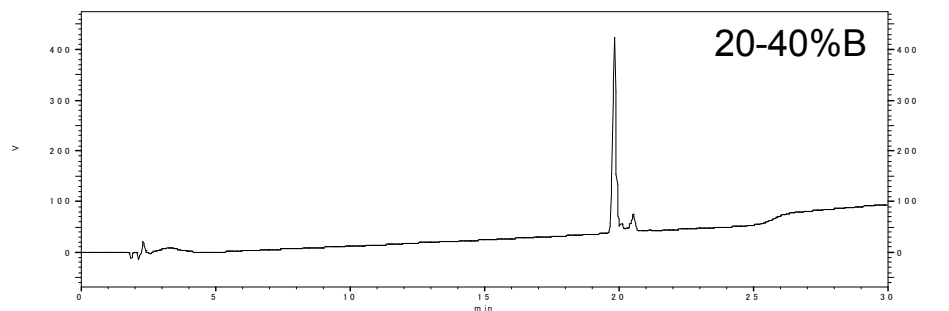
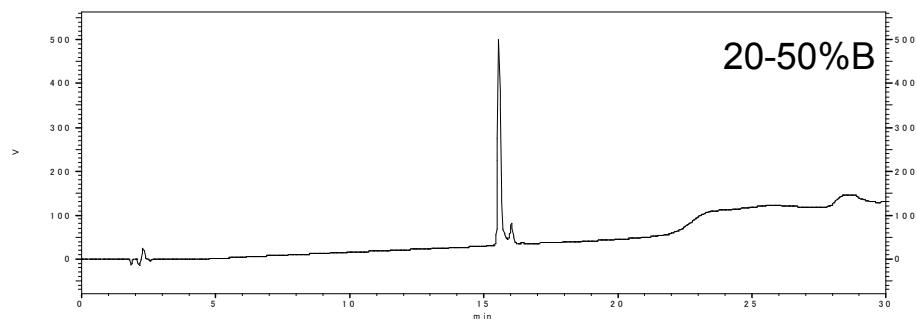
### Initial analytical conditions

Column : YMC-Pack C8, S-5 $\mu$ m,20nm (150mmX4.6mmI.D.)  
Flow rate : 1.0mL/min  
Eluent : A) water / TFA (100/0.1)  
          **B) \_\_\_\_\_ / TFA (100/0.1)**  
Detection : UV at 220 nm  
Temperature: ambient  
Sample : **Insulin (bovine/human=10/1)**





# Optimization of gradient condition with ACN

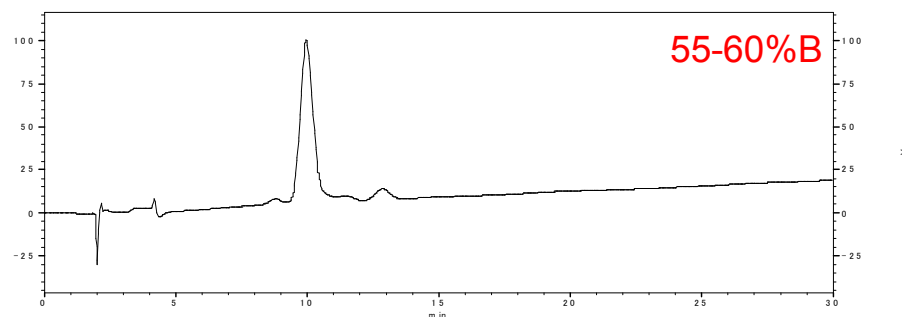
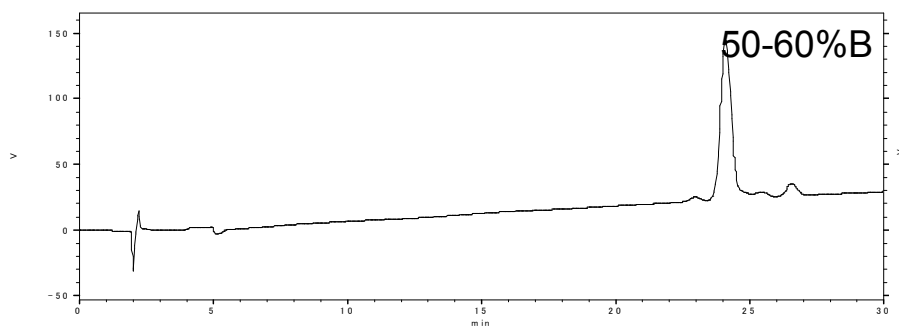
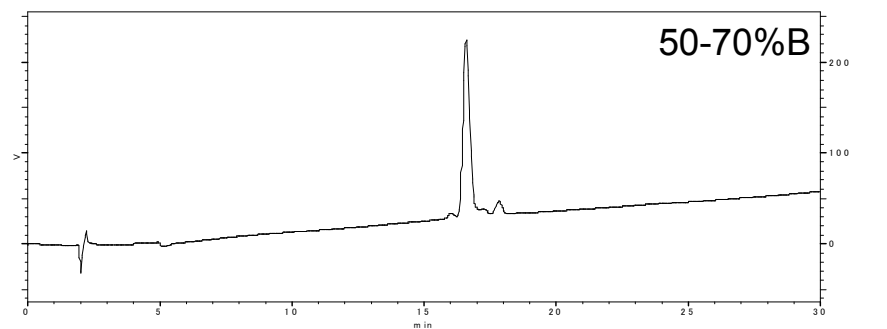
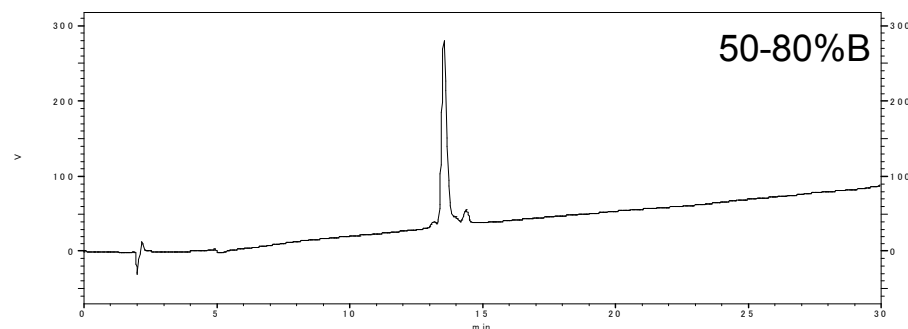


Appropriate optimization was not achieved in these analyses because of poor peak resolution between bovine and human.





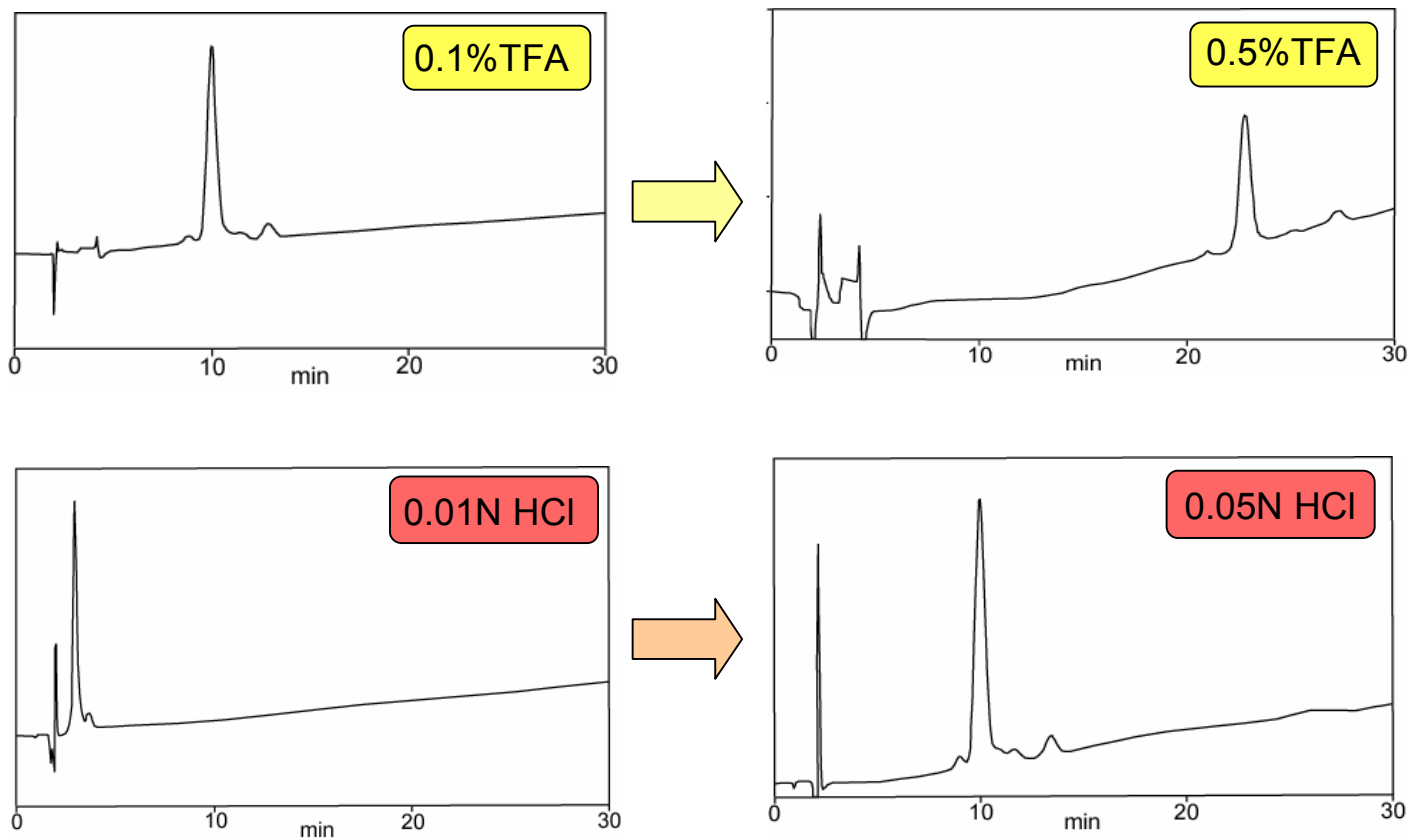
# Optimization of gradient condition with MeOH



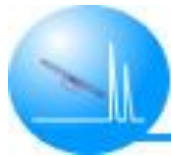
By using methanol as eluent, better separation was obtained in condition of 55-60%B solution. Methanol was better than ACN because it gave good separation, cost effective and better safety.



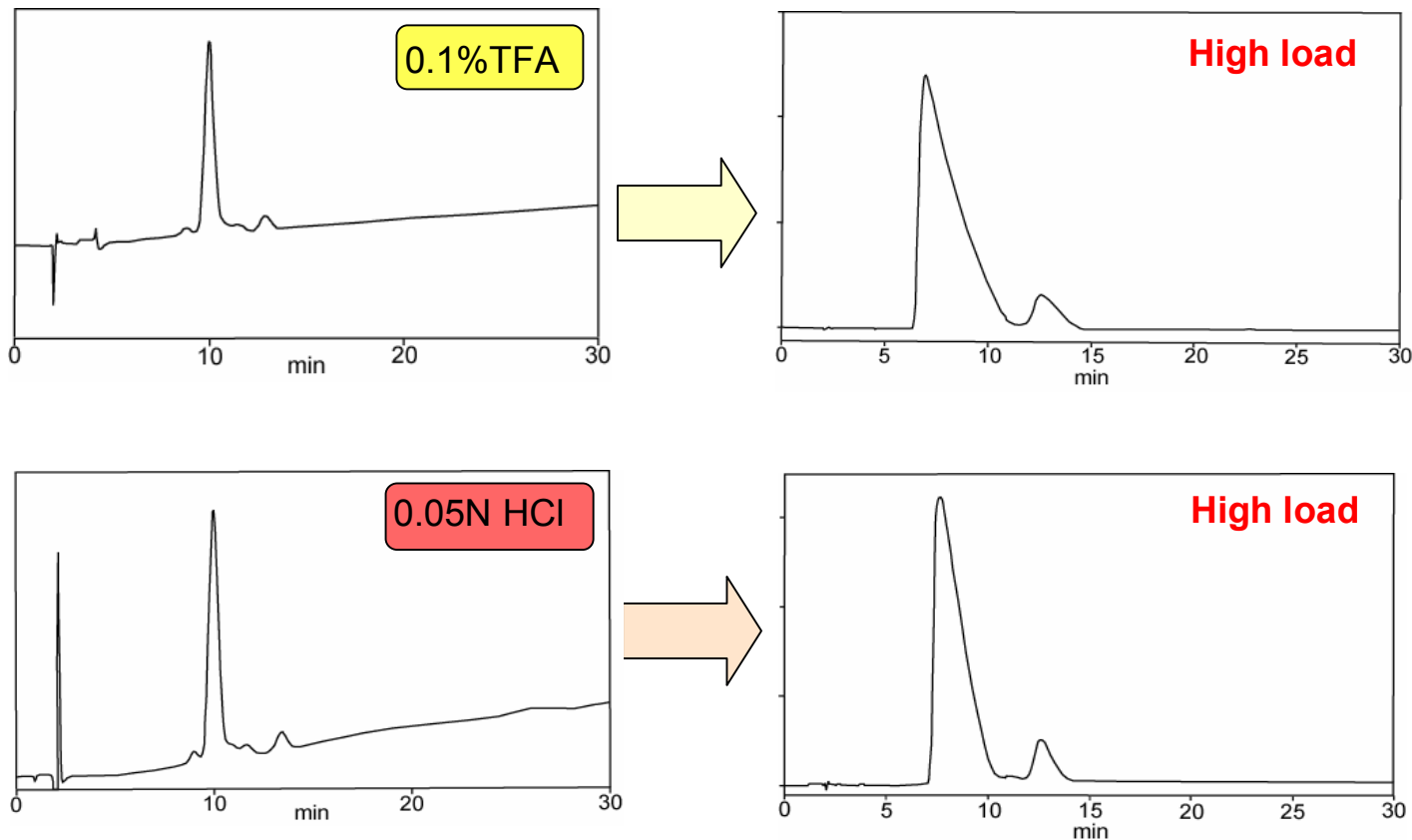
## Influences of *additive type and concentration*



Separations with 0.1% TFA and 0.05N HCl show appropriate retention time and good resolution.

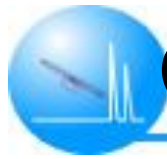


# Comparison of peak shape under high load

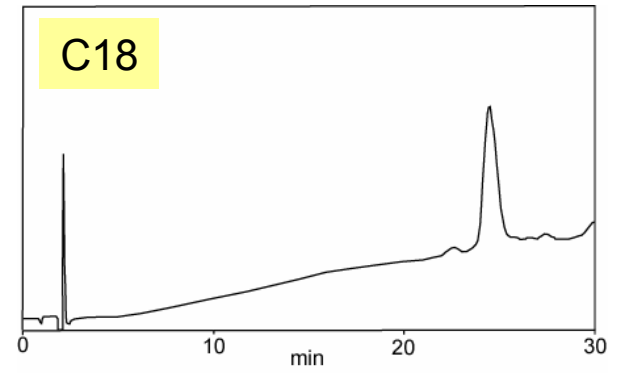
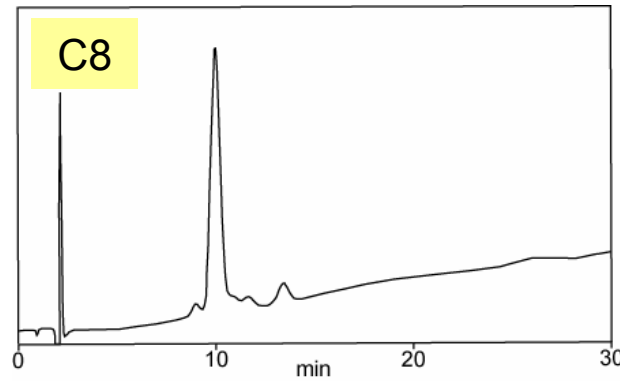
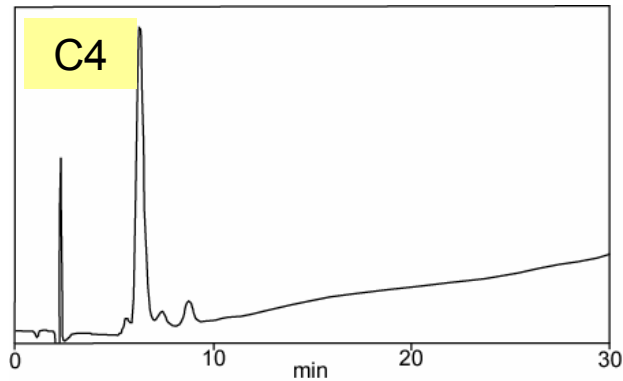


Using TFA additive shows broader than the case of HCl.

In terms of cost effective and peak shape, HCl was chosen as an additive.



# Comparison of packing material/functional group



	C4	C8	C18
Durability for acids	○	◎	◎
Cost performance	△	◎	○
Peak resolution	○	◎	○
Peak shape	◎	◎	○
Retention time	◎	◎	△

◎ Excellent,  
○ Good,  
△ Moderate

**C8 medium is best choice for the separation of insulin.**

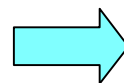
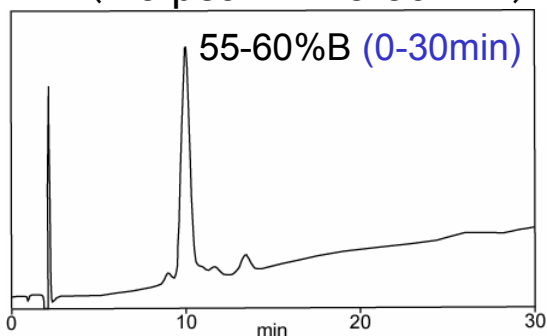




# Optimization of analysis time and flow rate

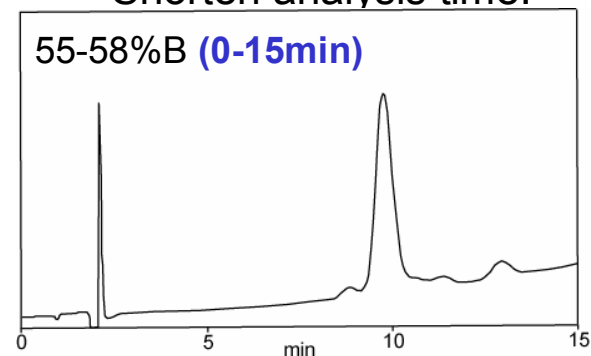
## 1) Optimized initial conditions

(No peak in 15-30 min)



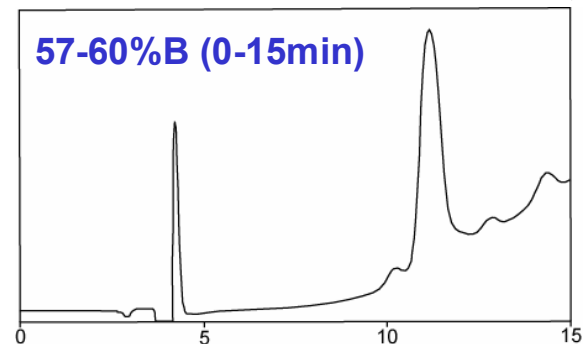
## 2) Half time of 1 cycle time

Shorten analysis time.



## 3) Fine optimization

Flow rate : 0.5 mL/min, gradient curve



Column : YMC-Pack C8, S-5 $\mu$ m, 20 nm (150mmX4.6mmI.D.)

Flow rate : 1.0mL/min  $\Rightarrow$  0.5 mL/min

Eluent : A) water / HCl (100/0.05N)

B) methanol / HCl (100/0.1)

Detection : UV at 220 nm

Temp. : ambienn

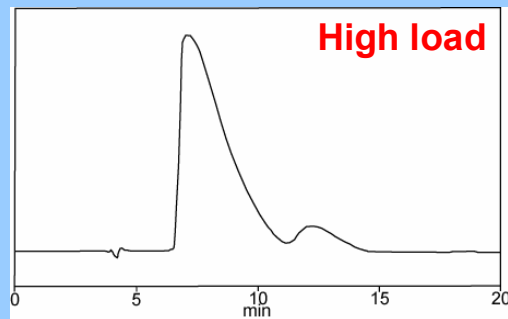
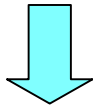
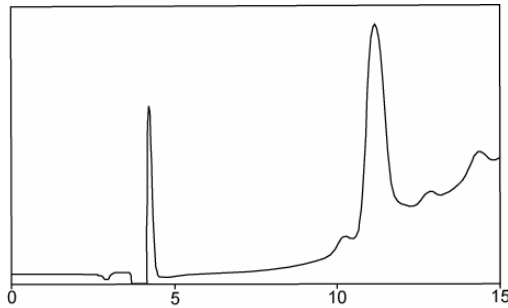
Sample : Insulin (bovine/human=10/1)

Fine optimization of gradient curve and flow rate, shorten analysis time and reduce eluent amount were achieved.

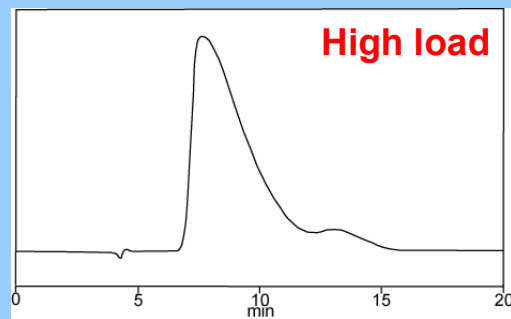
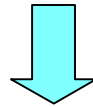
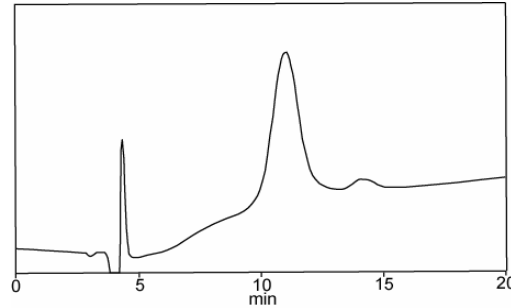


## Influence of particle size (C8, 20 nm)

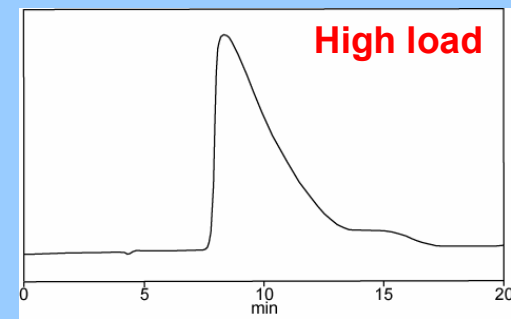
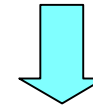
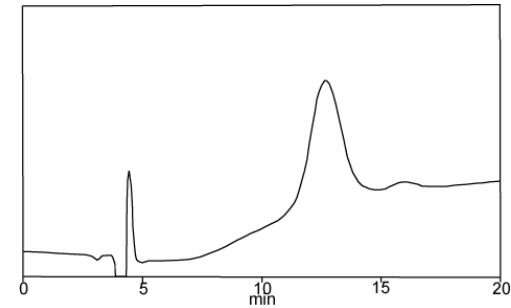
S-5  $\mu\text{m}$



S-10  $\mu\text{m}$



S-15  $\mu\text{m}$



In preparative, peak shape of each particle size are similar.

It is better to use larger particle size for cost effective production.



# Preparative conditions and cost performances

Conditions	Analytical	Preparative
Particle size	5 $\mu\text{m}$	15 $\mu\text{m}$
Packing material	C8, 20 nm	C8, 20 nm
Eluent	ACN / H <sub>2</sub> O/ TFA	MeOH / H <sub>2</sub> O/ HCl
Flow rate	1.0 mL/min	0.5 mL/min

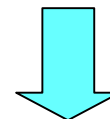
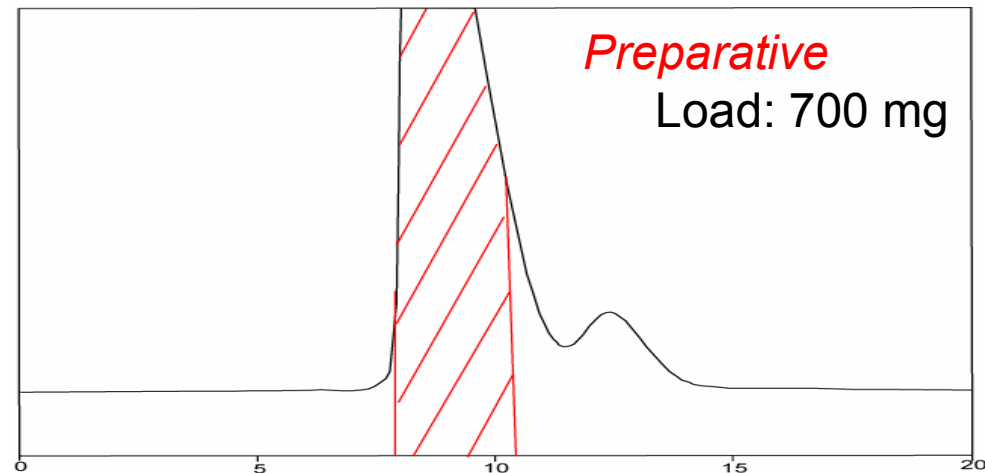
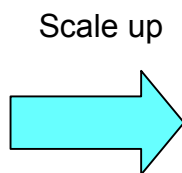
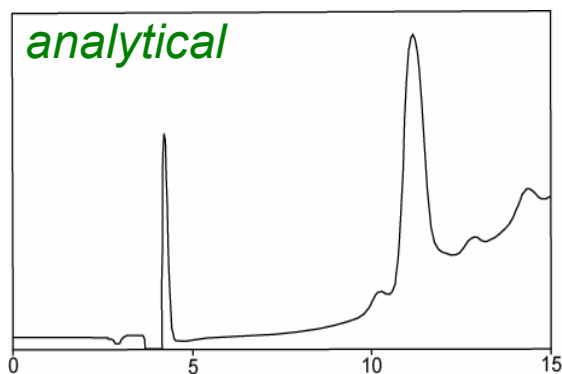
## Cost performance of each factor

Solvent (MeOH)	: 84% Decrease than ACN
Additive (HCl)	: 95% Decrease than TFA
Eluent (By reducing flow rate)	: 50% Decrease than initial condition
Preparative time of 1 cycle	: 50% Decrease than initial condition
Particle size (S-15 $\mu\text{m}$ )	: 95% Decrease than 5 $\mu\text{m}$



# Preparative separation of insulin (1)

## Scale up study (150mmX50mmI.D., DAU-50-700)



### Analytical conditions

Column	:YMC-Pack C8, 5 $\mu$ m, 20nm 150mmX4.6mmI.D.
Flow rate	:0.5mL/min
Eluent	: A) water / HCl (100/0.05N) B) methanol / HCl (100/0.05N) 57-60%B (0-15min, linear)
Detection	:UV at 220nm
Temperature	:ambient

### Preparative conditions

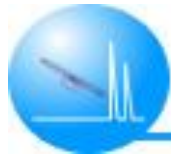
Column	:YMC * GEL C8, 15 $\mu$ m, 20nm 150mmX50mmI.D., (DAU-50-700)
Flow rate	:60mL/min
Eluent	: A) water / HCl (100/0.05N) B) methanol / HCl (100/0.05N) 57-60%B (0-15min, linear)
Detection	:UV at 220nm
Temperature	:ambient

### after fractionating

Purity	99%
Recovered amount	620 mg
Recovery	88%







## Preparative separation of insulin (2)

### *Loadability of insulin*

Loaded amount	200 mg	700 mg
Purity	99%	99%
Recovered amount	190 mg	620 mg
Recovery	95%	88%

The separation in 200 mg loaded shows high recovery, but low recovered amount. In production scale, higher loaded amount would give high recovery.



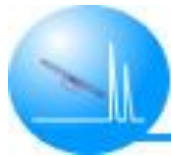
# Choice of column size

*3000 kg insulin purification per year*

Column size →	50 mml.D.	200 mml.D.	600 mml.D.
Loaded amount / day*	68 g	1056 g	4896 g
Product amount / year	24 kg	360 kg	<b>3560 kg</b>
Cost of packing material (ratio)	1.0	16	144


\* Cycle time: 15 min, Loading was performed 96 times per day.

To achieve expected production amount,  
it is necessary to use 600 mml.D. column.



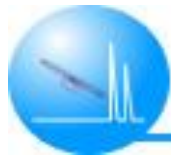
# Improvement of cost performance (1)

## *Comparison of cost performance in different conditions*

	Example conditions	Optimized conditions
1 cycle time	30 min (48 times/day)	15 min (96 times/day)
Eluent	Acetonitrile	Methanol
Flow rate*	17 L	8.6 L
Packing material	C18, 10 $\mu$ m	C8, 15 $\mu$ m
Eluent cost		<b>95% Decrease</b>
Cost of gel	Above conditions 	<b>90% Decrease</b>
Production efficiency		<b>100% Increase</b>

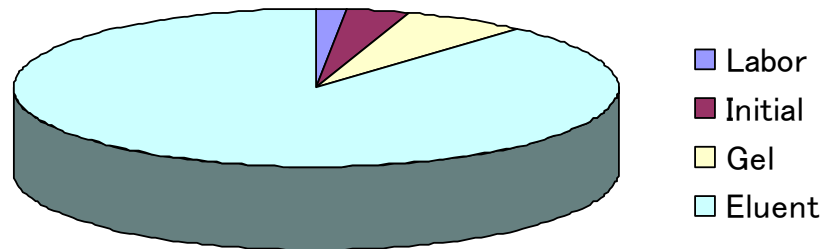
\*By using 600 mm I.D. column.

High flow rate and high column pressure cause not only increasing eluent amount but also increasing equipment cost.

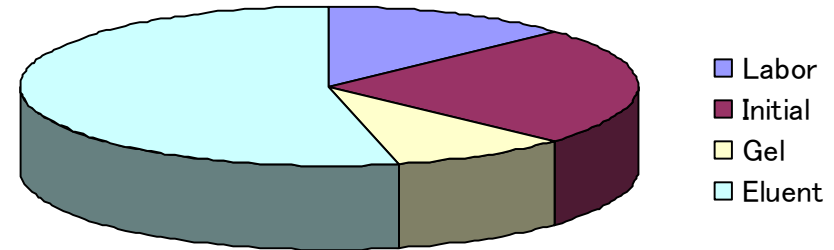


## Improvement of cost performance (2)

**Example conditions**



**Optimized conditions**



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<b>Total cost</b>	30,550,000 US\$	3,810,000 US\$
<b>Product amount/year</b>	1,780 kg	3,560 kg
<b>Total cost / Product 1 kg</b>	17,162 \$ / kg	1,070 \$ / kg
<b>Initial cost / Product 1 kg</b>	566 \$ / kg	278 \$ / kg
<b>Labor cost / Product 1 kg</b>	309 \$ / kg	149 \$ / kg
<b>Gel cost / Product 1 kg</b>	1132 \$ / kg	107 \$ / kg
<b>Eluent cost / Product 1 kg</b>	15,102 \$ / kg	631 \$ / kg

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By optimizing conditions, total cost is extremely lower than the example case.



## Summary

- In preparative production, by **choosing optimum conditions** as we shown this study, you can make **purification effectively**.
- It is important to **choose best combination of pore size, functional group and particle size** for the preparative purification of peptides and proteins.
- YMC can offer **not only various packing materials but also preparative products** (e.g. dynamic axial column, process equipments). We also offer the information of every stage of purification process.